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Condensation Formulas

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List of 22 Condensation Formulas

Condensation

1) Average Heat Transfer Coefficient for Condensation Inside Horizontal Tubes for Low Vapor Velocity

$$\text{fx } h^- = 0.555 \cdot \left(\frac{\rho_f \cdot (\rho_f - \rho_v) \cdot [g] \cdot h'_{fg} \cdot (k_f^3)}{L \cdot D_{\text{Tube}} \cdot (T_{\text{Sat}} - T_w)} \right)^{0.25}$$

[Open Calculator !\[\]\(a870788d6ed9b8fd294b7654a8c8526b_img.jpg\)](#)

ex

$$14.42554 \text{ W/m}^2 \cdot \text{K} = 0.555 \cdot \left(\frac{96 \text{ kg/m}^3 \cdot (96 \text{ kg/m}^3 - 0.5 \text{ kg/m}^3) \cdot [g] \cdot 3100000 \text{ J/kg} \cdot ((0.67 \text{ W/(m}^* \text{K)})^3)}{65 \text{ m} \cdot 9.71 \text{ m} \cdot (373 \text{ K} - 82 \text{ K})} \right)^{0.25}$$

2) Average Heat Transfer Coefficient for Film Condensation on Plate for Wavy Laminar Flow

$$\text{fx } h^- = 1.13 \cdot \left(\frac{\rho_f \cdot (\rho_f - \rho_v) \cdot [g] \cdot h_{fg} \cdot (k_f^3)}{L \cdot \mu_f \cdot (T_{\text{Sat}} - T_w)} \right)^{0.25}$$

[Open Calculator !\[\]\(6a9b39b98eb945faa14c645ec99e4eaa_img.jpg\)](#)

ex

$$116.0939 \text{ W/m}^2 \cdot \text{K} = 1.13 \cdot \left(\frac{96 \text{ kg/m}^3 \cdot (96 \text{ kg/m}^3 - 0.5 \text{ kg/m}^3) \cdot [g] \cdot 2260000 \text{ J/kg} \cdot ((0.67 \text{ W/(m}^* \text{K)})^3)}{65 \text{ m} \cdot 0.029 \text{ N}^* \text{s/m}^2 \cdot (373 \text{ K} - 82 \text{ K})} \right)^{0.25}$$

3) Average Heat Transfer Coefficient for Laminar Film Condensation of Tube


$$\text{fx } h^- = 0.725 \cdot \left(\frac{\rho_f \cdot (\rho_f - \rho_v) \cdot [g] \cdot h_{fg} \cdot (k_f^3)}{D_{\text{Tube}} \cdot \mu_f \cdot (T_{\text{Sat}} - T_w)} \right)^{0.25}$$

[Open Calculator !\[\]\(235bfe13ebf007ce2eea9e689707fac7_img.jpg\)](#)

ex

$$119.8098 \text{ W/m}^2 \cdot \text{K} = 0.725 \cdot \left(\frac{96 \text{ kg/m}^3 \cdot (96 \text{ kg/m}^3 - 0.5 \text{ kg/m}^3) \cdot [g] \cdot 2260000 \text{ J/kg} \cdot ((0.67 \text{ W/(m}^* \text{K)})^3)}{9.71 \text{ m} \cdot 0.029 \text{ N}^* \text{s/m}^2 \cdot (373 \text{ K} - 82 \text{ K})} \right)^{0.25}$$




4) Average Heat Transfer Coefficient for Laminar Film Condensation on Outside of Sphere 

$$fx \quad h^- = 0.815 \cdot \left(\frac{\rho_f \cdot (\rho_f - \rho_v) \cdot [g] \cdot h_{fg} \cdot (k_f^3)}{D_{\text{Sphere}} \cdot \mu_f \cdot (T_{\text{Sat}} - T_w)} \right)^{0.25}$$

Open Calculator 

ex

$$134.6481 \text{W/m}^2 \cdot \text{K} = 0.815 \cdot \left(\frac{96 \text{kg/m}^3 \cdot (96 \text{kg/m}^3 - 0.5 \text{kg/m}^3) \cdot [g] \cdot 2260000 \text{J/kg} \cdot ((0.67 \text{W}/(\text{m} \cdot \text{K}))^3)}{9.72 \text{m} \cdot 0.029 \text{N} \cdot \text{s}/\text{m}^2 \cdot (373 \text{K} - 82 \text{K})} \right)^{0.25}$$

5) Average Heat Transfer Coefficient for Vapor Condensing on Plate 

$$fx \quad h^- = 0.943 \cdot \left(\frac{\rho_f \cdot (\rho_f - \rho_v) \cdot [g] \cdot h_{fg} \cdot (k_f^3)}{L \cdot \mu_f \cdot (T_{\text{Sat}} - T_w)} \right)^{0.25}$$

Open Calculator 

ex

$$96.8819 \text{W/m}^2 \cdot \text{K} = 0.943 \cdot \left(\frac{96 \text{kg/m}^3 \cdot (96 \text{kg/m}^3 - 0.5 \text{kg/m}^3) \cdot [g] \cdot 2260000 \text{J/kg} \cdot ((0.67 \text{W}/(\text{m} \cdot \text{K}))^3)}{65 \text{m} \cdot 0.029 \text{N} \cdot \text{s}/\text{m}^2 \cdot (373 \text{K} - 82 \text{K})} \right)^{0.25}$$

6) Average Heat Transfer Coefficient given Reynolds Number and Properties at Film Temperature 

$$fx \quad h^- = \frac{0.026 \cdot \left(P_f^{\frac{1}{3}}\right) \cdot (\text{Re}_m^{0.8}) \cdot (K_f)}{D_{\text{Tube}}}$$

Open Calculator 

$$ex \quad 0.782819 \text{W/m}^2 \cdot \text{K} = \frac{0.026 \cdot ((0.95)^{\frac{1}{3}}) \cdot ((2000)^{0.8}) \cdot (0.68 \text{W}/(\text{m} \cdot \text{K}))}{9.71 \text{m}}$$


7) Condensation Number 

$$fx \quad Co = (h^-) \cdot \left(\left(\frac{(\mu_f)^2}{(k^3) \cdot (\rho_f) \cdot (\rho_f - \rho_v) \cdot [g]} \right)^{\frac{1}{3}} \right)$$

Open Calculator 

$$ex \quad 0.023802 = (115 \text{W/m}^2 \cdot \text{K}) \cdot \left(\left(\frac{(0.029 \text{N} \cdot \text{s}/\text{m}^2)^2}{((10.18 \text{W}/(\text{m} \cdot \text{K}))^3) \cdot (96 \text{kg/m}^3) \cdot (96 \text{kg/m}^3 - 0.5 \text{kg/m}^3) \cdot [g]} \right)^{\frac{1}{3}} \right)$$



8) Condensation Number for Horizontal Cylinder 

fx $Co = 1.514 \cdot \left((Re_f)^{-\frac{1}{3}} \right)$

Open Calculator 


ex $0.226162 = 1.514 \cdot \left((300)^{-\frac{1}{3}} \right)$

9) Condensation Number for Vertical Plate 

fx $Co = 1.47 \cdot \left((Re_f)^{-\frac{1}{3}} \right)$

Open Calculator 


ex $0.219589 = 1.47 \cdot \left((300)^{-\frac{1}{3}} \right)$

10) Condensation Number given Reynolds Number 

fx $Co = \left((C)^{\frac{4}{3}} \right) \cdot \left(\left(\frac{4 \cdot \sin(\Phi) \cdot \left(\left(\frac{A_{cs}}{P} \right) \right)^{\frac{1}{3}}}{L} \right) \right) \cdot \left((Re_f)^{-\frac{1}{3}} \right)$

Open Calculator 

ex $0.139312 = \left((1.5)^{\frac{4}{3}} \right) \cdot \left(\left(\frac{4 \cdot \sin(1.55\text{rad}) \cdot \left(\left(\frac{25\text{m}^2}{9.6\text{m}} \right) \right)^{\frac{1}{3}}}{65\text{m}} \right) \right) \cdot \left((300)^{-\frac{1}{3}} \right)$

11) Condensation Number when Turbulence is Encountered in Film 

fx $Co = 0.0077 \cdot \left((Re_f)^{0.4} \right)$

Open Calculator 

ex $0.075394 = 0.0077 \cdot \left((300)^{0.4} \right)$

12) Film Thickness given Mass Flow of Condensate 

fx $\delta = \left(\frac{3 \cdot \mu_f \cdot \dot{m}}{\rho_L \cdot (\rho_L - \rho_v) \cdot [g]} \right)^{\frac{1}{3}}$

Open Calculator 

ex $0.002316\text{m} = \left(\frac{3 \cdot 0.029\text{N*s/m}^2 \cdot 1.40\text{kg/s}}{1000\text{kg/m}^3 \cdot (1000\text{kg/m}^3 - 0.5\text{kg/m}^3) \cdot [g]} \right)^{\frac{1}{3}}$



13) Film Thickness in Film Condensation 

$$\text{fx } \delta = \left(\frac{4 \cdot \mu_f \cdot k \cdot x \cdot (T_{\text{Sat}} - T_w)}{[g] \cdot h_{fg} \cdot (\rho_L) \cdot (\rho_L - \rho_v)} \right)^{0.25}$$

Open Calculator 


$$\text{ex } 0.000982\text{m} = \left(\frac{4 \cdot 0.029\text{N}^*\text{s}/\text{m}^2 \cdot 10.18\text{W}/(\text{m}^*\text{K}) \cdot 0.06\text{m} \cdot (373\text{K} - 82\text{K})}{[g] \cdot 2260000\text{J}/\text{kg} \cdot (1000\text{kg}/\text{m}^3) \cdot (1000\text{kg}/\text{m}^3 - 0.5\text{kg}/\text{m}^3)} \right)^{0.25}$$

14) Heat Transfer Coefficient for Condensation on Flat Plate for Nonlinear Temperature Profile in Film 

$$\text{fx } h'_{fg} = (h_{fg} + 0.68 \cdot c \cdot (T_{\text{Sat}} - T_w))$$

Open Calculator 


$$\text{ex } 3.1\text{E}^6\text{J}/\text{kg} = (2260000\text{J}/\text{kg} + 0.68 \cdot 4184\text{J}/(\text{kg}^*\text{K}) \cdot (373\text{K} - 82\text{K}))$$

15) Heat Transfer Rate for Condensation of Superheated Vapors 

$$\text{fx } q = h \cdot A_{\text{plate}} \cdot ((T_s') - T_w)$$

Open Calculator 


$$\text{ex } 28658\text{W} = 115\text{W}/\text{m}^2^*\text{K} \cdot 35.6\text{m}^2 \cdot (89\text{K} - 82\text{K})$$

16) Mass Flow of Condensate through any X Position of Film 


$$\text{fx } \dot{m} = \frac{\rho_L \cdot (\rho_L - \rho_v) \cdot [g] \cdot (\delta^3)}{3 \cdot \mu_f}$$

Open Calculator 


$$\text{ex } 1.406851\text{kg}/\text{s} = \frac{1000\text{kg}/\text{m}^3 \cdot (1000\text{kg}/\text{m}^3 - 0.5\text{kg}/\text{m}^3) \cdot [g] \cdot ((0.00232\text{m})^3)}{3 \cdot 0.029\text{N}^*\text{s}/\text{m}^2}$$

17) Mass Flow Rate through Particular Section of Condensate Film given Reynolds Number of Film 

$$\text{fx } \dot{m}_1 = \frac{\text{Re}_f \cdot P \cdot \mu}{4}$$

Open Calculator 

$$\text{ex } 7200\text{kg}/\text{s} = \frac{300 \cdot 9.6\text{m} \cdot 10\text{N}^*\text{s}/\text{m}^2}{4}$$

18) Reynolds Number for Condensate Film 

$$\text{fx } \text{Re}_f = \frac{4 \cdot \dot{m}_1}{P \cdot \mu}$$

Open Calculator 

$$\text{ex } 300 = \frac{4 \cdot 7200\text{kg}/\text{s}}{9.6\text{m} \cdot 10\text{N}^*\text{s}/\text{m}^2}$$



19) Reynolds Number using Average Heat Transfer Coefficient for Condensate Film 

Open Calculator 

$$fx \quad Re_f = \left(\frac{4 \cdot h^- \cdot L \cdot (T_{Sat} - T_w)}{h_{fg} \cdot \mu_f} \right)$$

$$ex \quad 132.7571 = \left(\frac{4 \cdot 115W/m^2 \cdot K \cdot 65m \cdot (373K - 82K)}{2260000J/kg \cdot 0.029N^*s/m^2} \right)$$

20) Viscosity of Film given Mass Flow of Condensate 

Open Calculator 

$$fx \quad \mu_f = \frac{\rho_L \cdot (\rho_L - \rho_v) \cdot [g] \cdot (\delta^3)}{3 \cdot \dot{m}}$$

$$ex \quad 0.029142N^*s/m^2 = \frac{1000kg/m^3 \cdot (1000kg/m^3 - 0.5kg/m^3) \cdot [g] \cdot ((0.00232m)^3)}{3 \cdot 1.40kg/s}$$

21) Viscosity of Film given Reynolds Number of Film 

Open Calculator 

$$fx \quad \mu_f = \frac{4 \cdot \dot{m}_1}{P \cdot Re_f}$$

$$ex \quad 10N^*s/m^2 = \frac{4 \cdot 7200kg/s}{9.6m \cdot 300}$$

22) Wetted Perimeter given Reynolds Number of Film 

Open Calculator 

$$fx \quad P = \frac{4 \cdot \dot{m}_1}{Re_f \cdot \mu}$$

$$ex \quad 9.6m = \frac{4 \cdot 7200kg/s}{300 \cdot 10N^*s/m^2}$$















Variables Used

- A_{CS} Cross Sectional Area of Flow (Square Meter)
- A_{plate} Area of Plate (Square Meter)
- c Specific Heat Capacity (Joule per Kilogram per K)
- C Constant for Condensation Number
- Co Condensation Number
- D_{Sphere} Diameter of Sphere (Meter)
- D_{Tube} Diameter of Tube (Meter)
- h^- Average Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- h_{fg} Latent Heat of Vaporization (Joule per Kilogram)
- h'_{fg} Corrected Latent Heat of Vaporization (Joule per Kilogram)
- k Thermal Conductivity (Watt per Meter per K)
- k_f Thermal Conductivity of Film Condensate (Watt per Meter per K)
- K_f Thermal Conductivity at Film Temperature (Watt per Meter per K)
- L Length of Plate (Meter)
- \dot{m} Mass Flow Rate (Kilogram per Second)
- \dot{m}_1 Mass Flow of Condensate (Kilogram per Second)
- P Wetted Perimeter (Meter)
- P_f Prandtl Number at Film Temperature
- q Heat Transfer (Watt)
- Re_f Reynolds Number of Film
- Re_m Reynolds Number for Mixing
- T_s' Saturation Temperature for Superheated Vapor (Kelvin)
- T_{Sat} Saturation Temperature (Kelvin)
- T_w Plate Surface Temperature (Kelvin)
- x Height of Film (Meter)
- δ Film Thickness (Meter)
- μ Viscosity of Fluid (Newton Second per Square Meter)
- μ_f Viscosity of Film (Newton Second per Square Meter)
- ρ_f Density of Liquid Film (Kilogram per Cubic Meter)
- ρ_L Density of Liquid (Kilogram per Cubic Meter)
- ρ_v Density of Vapor (Kilogram per Cubic Meter)
- Φ Inclination Angle (Radian)



Constants, Functions, Measurements used

- **Constant:** [g], 9.80665 Meter/Second²
Gravitational acceleration on Earth
- **Function:** sin, sin(Angle)
Trigonometric sine function
- **Measurement:** **Length** in Meter (m)
Length Unit Conversion 
- **Measurement:** **Temperature** in Kelvin (K)
Temperature Unit Conversion 
- **Measurement:** **Area** in Square Meter (m²)
Area Unit Conversion 
- **Measurement:** **Power** in Watt (W)
Power Unit Conversion 
- **Measurement:** **Angle** in Radian (rad)
Angle Unit Conversion 
- **Measurement:** **Thermal Conductivity** in Watt per Meter per K (W/(m*K))
Thermal Conductivity Unit Conversion 
- **Measurement:** **Specific Heat Capacity** in Joule per Kilogram per K (J/(kg*K))
Specific Heat Capacity Unit Conversion 
- **Measurement:** **Mass Flow Rate** in Kilogram per Second (kg/s)
Mass Flow Rate Unit Conversion 
- **Measurement:** **Heat Transfer Coefficient** in Watt per Square Meter per Kelvin (W/m²*K)
Heat Transfer Coefficient Unit Conversion 
- **Measurement:** **Dynamic Viscosity** in Newton Second per Square Meter (N*s/m²)
Dynamic Viscosity Unit Conversion 
- **Measurement:** **Density** in Kilogram per Cubic Meter (kg/m³)
Density Unit Conversion 
- **Measurement:** **Latent Heat** in Joule per Kilogram (J/kg)
Latent Heat Unit Conversion 



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